

Greene & Donoho

Duty Trial of a
Producer-Gas-Engine-Driven
26-Inch Centrifugal Pump

Mechanical Engineering

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DUTY TRIAL OF A PRODUCER-GAS-ENGINE-DRIVEN
26-INCH CENTRIFUGAL PUMP

BY

William Bertram Greene
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THESIS FOR THE DEGREE OF BACHELOR OF SCIENCE
IN MECHANICAL ENGINEERING

IN THE
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OF THE
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June 1, 1908

THIS IS TO CERTIFY THAT THE THESIS PREPARED UNDER MY SUPERVISION BY

WILLIAM BERTRAM GREENE EARL WILLOUGHBY DONOHO

ENTITLED DUTY TRIAL OF A PRODUCER-GAS-ENGINE-DRIVEN 26-INCH
CENTRIFUGAL PUMP

IS APPROVED BY ME AS FULFILLING THIS PART OF THE REQUIREMENTS FOR THE

DEGREE OF Bachelor of Science in Mechanical Engineering

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Instructor in Charge.

APPROVED:

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HEAD OF DEPARTMENT OF Mechanical Engineering



OUTLINE OF THESIS.

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DUTY TRIAL OF A PRODUCER GAS ENGINE
DRIVEN 26" CENTRIFUGAL PUMP.

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DUTY TRIAL OF A PRODUCER GAS ENGINE
DRIVEN 26" CENTRIFUGAL PUMP.

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INTRODUCTION.

This thesis consists of a commercial test made on a producer gas engine driven centrifugal pump at Pekin, Illinois. The plant is new and the tests herein discussed served in a measure as contract acceptance tests. The plant is owned by the Pekin and La Marge Drainage District, an organization of farmers formed for the purpose of erecting and operating a pump to drain the water from their low farm land into the Illinois river.

OBJECT OF TESTS.

The object of these tests, as indicated above is to determine the conformity of the actual efficiency of the pump with the manufacturer's guarantee.

NUMBER OF TESTS.

On March 25 and 26 tests were made on the complete plant, each test lasting about eight hours. During the first test the engine stopped once and several times it slowed down, and accordingly the second test was run in hopes of getting better operation of the engine. Between the two tests the engine main bearings and reciprocating parts were carefully examined and adjusted. A one hour test for the mechanical efficiency



of the engine was run on March 27 to permit an analysis of the performance of the component parts of the installation.

DESCRIPTION OF PLANT.

PUMP.

The pump tested was a Lawrence Double Suction 26" Centrifugal Pump, run at 210 R. P. M. It was driven thru a continuous rope drive of 1 1/4" rope of nine turns as shown on drawing, page . The pump was located about two feet above the suction level in a small "lean to" which adjoined the engine house. The engine house floor was seven feet above the pump.

ENGINE.

A vertical three cylinder four cycle 14" x 15" Webber engine rated at 125 H.P. was used to run the pump. Ignition was taken care of by a small magneto; governing was done by means of throttling the mixture.

PRODUCER.

Two producers had been installed with one scrubber between them; only one of the producers was needed for operation and the same one was used continuously. They were Webber Suction Producers rated at 125 H.P.

ACCESSARIES.

A jack shaft over head could either be connected to the large engine or it could be run by a small gasoline engine. To this were connected a suction fan for starting the producer, a small rotary pump for circulating the cooling water and a



small generator for lighting the plant. An air compressor was connected directly to the gasoline engine and pumped air into a tank; by means of this compressed air the large engine was started.

TESTS.

The following observations were made at ten minute intervals thruout the test with exception of "General Data" which was taken every hour.

1. DUTY TRIALS.

General Data.

1. Barometer reading.
2. External air temperature.
3. Engine room temperature.

Engine performance.

4. Temperature of jacket water, initial.
5. Temperature of jacket water final.
6. Temperature of gas to engine.
7. Temperature of exhaust.
8. Weight of jacket water per minute.
9. Weight of coal to producer.
10. Weight of ash.
11. R. P. M. of Engine.
12. F. P. M. of engine.
13. Indicator diagram, Cylinder No. 1.
14. Indicator diagram, Cylinder No. 2.
15. Indicator diagram, Cylinder No. 3.



Pump Performance.

16. Temperature of Suction Water.
17. Suction head.
18. Delivery head.
19. Velocity head in suction pipe, Pitot tube reading.
20. Velocity head in discharge pipe, Pitot tube reading.
21. R. P. M. of pump.

2. MECHANICAL EFFICIENCY TEST.

General Data.

1. Barometer reading.
2. External air temperature.
3. Engine room temperature.

Engine Performance.

4. Temperature of gas to engine.
5. Temperature of exhaust gas.
6. Temperature of jacket water, initial.
7. Temperature of jacket water, final.
8. Indicator diagram, Cylinder No. 1.
9. Indicator diagram, Cylinder No. 2.
10. Indicator diagram, Cylinder No. 3.
11. R. P. M. of engine.
12. E. P. M. of engine.
13. Net Weight of brake on scales.

METHOD.

In order to determine the mechanical efficiency of



the pump the combined efficiency of the engine and pump had first to be obtained by taking the ratio of the water horse power to the indicated horse power. This ratio divided by the mechanical efficiency of the engine gives the pump efficiency including transmission.

TO GET PLANT EFFICIENCY.

Samples of coal and ash were taken for testing and all coal put into hopper and all ash from the grates was weighed for the purpose of getting the thermal efficiency of the plant. The thermal efficiency is the ratio of the delivered horse-power to the horse power equivalent to the B. T. U. delivered in the coal to the producer, correction being made for heat in refuse.

TEMPERATURES.

All temperatures of gas, water and air were taken merely for purposes of general information as a heat balance or analysis was impossible in the absence of a gas analysis.

JACKET WATER.

The weight of jacket water per minute was obtained by timing the flow into a bucket with a stop watch and weighing the same. This did not enter into the final calculations for the reasons already given of the impracticability of a heat balance.

INDICATOR CARDS.

Indicator springs were calibrated after the test was made. The reducing motion consisted of a long cord passing across the top of the engine where the indicators were located,



and guided by pulleys down to the end of the shaft, where there was an arrangement that enabled an operator to hook the cord onto any one of three cranks which worked in phase with the different cylinders. The accompanying sketch, page , will better show the arrangement.

R.P.M. OF ENGINE.

This was obtained by means of a tachometer which had been calibrated with an ordinary speed counter.

R.P.M. OF PUMP.

This was obtained by multiplying the engine R.P.M. by the velocity ratio of the two pulleys.

VELOCITY HEAD.

Calibrated Pitot tubes were placed in the discharge and in the suction pipe and were read simultaneously. The reading of the one in discharge pipe was accepted as standard as it was placed in a straight section of pipe and the other had necessarily been placed near a bend.

SUCTION HEAD.

This was obtained by means of a vacuum gage.

DISCHARGE HEAD.

This was measured with a mercury column connected by tubing to the discharge end of the pump.

RESULTS.

From the above observations and from the coal and ash analyses the following results were calculated.

Item.	Trial No. 1. Mar. 25, '08	Trial No. 2. Mar. 26, '08
1. Duration of trial, hours,	7.4	7.58
2. Atmospheric pressure, lbs. per sq. in. (Read- ing No. 1 x .493	14.0	14.15
3. Average external air temperature (From read- ing No. 2)	66.5°F.	65.2°F.
4. Average engine room tempera- ture. (From reading No.3)	70.6°F.	70.1°F.
5. Average temperature of gas to Engine. (From reading No. 6)	68.7°F.	72.3°F.
6. Average temperature exhaust gases. (From Reading No.7)	208.4°F.	254.6°F.
7. Average initial temperature of jacket water. (From reading No. 4)	54.0°F.	64.3°F.
8. Average final temperature of jacket water (From reading No. 5)	100.5°F.	141.8°F.
9. Average temperature difference. ("Item 8" - "Item 7")	46.5°F.	77.5°F.

Trial No. 1. Trial No. 2.

10.	Average R.P.M. of engine		
	(From Reading No. 11)	284	295
11.	Average Explosion per minute.		
	("Item 10" ÷ 2)	142	147.5
12.	I.H.P. cylinder No. 1.		
	(.00584 x M.E.P. x "Item 11")	18.1	27
13.	I.H.P. cylinder No. 2.	17.5	21.9
14.	I.H.P. cylinder No. 3.	25.6	24.1
15.	Total I.H.P. for engine.		
	("Item 12" "Item 13"		
	"Item 14")	61.2	73
16.	Average temperatures of suction		
	water, T. (From reading		
	No. 16)	51.80	59.40
17.	Average velocity of flow in suc-		
	tion pipe in ft. per sec. V'		
	(V' = $2 g h$; h, velocity		
	head in pitot tube, in feet		
	of water from reading No. 19)	8.04	7.96
18.	Average R.P.M. of pump.		
	("Item 10" x 54/40)	210	219
19.	Average velocity of flow in dis-		
	charge pipe in ft. per sec,		
	V. V = $.975 \ 2 g h$)	7.53	7.56

Trial No. 1. Trial No. 2.

20. Average velocity. ("Item 17"		
"Item 19") ÷ 2)	8.09	7.76
21. Water pumped, cubic feet per		
second. Q. (Q = V x A, A =		
area discharge pipe)	27.7	27.8
22. Water pumped, gallons per minute,		
G.; (G = tO x Q x D, D = gallons		
per cubic foot at temperature		
T, "Item 16")	12,400	12,450
23. Water pumped, pounds per second.		
("Item 19" x weight per cubic		
foot at temperature, T)	1732	1739
24. Total gage head, feet.		
(Average reading No. 17 and		
No. 18)	9.06	8.43
25. Total level head, feet.		
(Measurement)	8.08	8.08
26. Water horse power. ("Item 23"		
all (Reading 17 by 5 Reading 18))	28.6	27.61
27. Effective horse power.		
<u>"Item 27" x "Item 25"</u>	26.4	26.5
550		
28. Capacity of pump, gallons per 24		
hours. "Item 22" x 60 x 24.	17840000	17910000
29. Total coal burned per hour as		
fired. Reading No.9 ÷ Item 1.	117.2	93.2

Trial No. 1. Trial No. 2.

30.	Total coal burned, lbs per I.H.P. hour. "Item 29 ÷ "Item 15"	1.92	1.275
31.	Total coal burned, lbs. per B.H.P. hr. "Item 30" ÷ .786, Mech. eff.	2.44	1.623
32.	Total coal burned, lbs. per I.H.P. hour. "Item 29" ÷ "Item 26"	4.1	3.39
33.	Total coal burned, lbs. per ef- fective horse power hour. "Item 29" ÷ "Item 27"	4.44	3.52
34.	Total ash and refuse per hour,	35.20	21.25
35.	Coal analysis.		
	Moisture,	2.15%	1.43%
	Ash	15.83	15.25
	Sulphur	.94	.91
	Hydrogen	2.80	2.84
	Carbon	75.68	76.76
	Nitrogen	.85	.85
	Oxygen	1.75	1.96
	B.T.U. per lb. of coal as fired (Parr calorimeter)	12,330	12,569
36.	Ash analysis.		
	Moisture	1.10%	.64%
	Volitile matter	45.64	42.54

	Trial No. 1.	Trial No. 2.
36. (Continued)		
Fixed carbon	53.26	56.82
Ash		
B.T.U. (calculated)	6861	6417
37. B.T.U. per hour supplied to the producer. "Item 29 x "Item 35"	1,445,000	1,171,500
38. B.T.U. per hour supplied to producer and rejected in refuse. "Item 34" x "Item 36"	241,500	136,350
39. Net B.T.U. evolved per hour in producer. "Item 37" - "Item 38"	1,203,500	1,035,150
40. B.T.U. per I.H.P. hr. "Item 39" ÷ "Item 15"	23,600	16,045
41. B.T.U. per B.H.P. hr. "Item 39" ÷ (.786, Mech. eff. x I.H.P.)	30,040	20,410
42. B.T.U. per W.H.P. hr. "Item 39" ÷ "Item 26"	48,850	42,820
43. B.T.U. per effective H.P. hr. "Item 39" ÷ "Item 27"	54,800	45,400
44. Pump Duty. (Foot-lbs. of work done per 1,000,000 B.T.U. supplied bases upon coal as fired and pump horse-power.	39,220,000	44,750,000

Trial No. 1. Trial No. 2.

45. Overall pumping efficiency.

(Ratio of heat equivalent
of W.H.P. to "Item 39")

46. Overall plant efficiency. (Ratio
of heat equivalent of effec-

tive horse power to "Item 39) 4.66% 5.75%

47. Potential efficiency of Pro-

ducer, transmission, engine
and pump. "Item 39" and

W.H.P. 6.05% 6.72%

48. Efficiency ratio, Mech. eff.

(B.H.P. ÷ I.H.P.) 78.6% 78.6%

49. Efficiency ratio. (W.H.P. ÷ I.H.P) 46.7% 36.6%

50. Efficiency ratio. (Effective

horse power ÷ I.H.P.) 43.3% 36.3%

SUMMARY OF RESULTS.

The following table shows significant results as taken from the previous table, compared with normal results which should be expected.

Item.	Trial No.1.	Trial No.2.	Normal.
1. Duration of trial, hrs.	7.8	7.28	
15. Total average I.H.P.	61.2	73	147
48. Mechanical efficiency of engine.	78.6%	78.6%	85%
Estimated B.H.P.	48.1	57.3	125
17. Velocity in discharge pipe, feet per second.	8.64	7.96	10
22. Water pumped, gallons per minute.	12,400	12,450	16,650
26. W.H.P.	28.6	26.61	35.4
27. Effective horse power	26.4	26.50	34
28. Capacity of pump, gallons per 24 hrs.	17,8740,000	17,910,000	24000000
31. Coal burned per B.H.P:	2.44	1.62	1.25
35. B.T.U. per pound of coal.	12,330	12,569	12,500
44. Pump Duty.	39,2200,000	46,580,000	
49. Efficiency ratio, W.H.P. ÷ I.H.P.	46.7%	36.6%	80%
50. Efficiency ratio. Effec- tive H.P. ÷ I.H.P.	43.3%	36.37%	75%

CONCLUSIONS.

Owing to rather unsatisfactory performance of the engine and producer during test, the results as a whole probably err as high as 5%. Still with the results obtained and the record of performance the following conclusions may be drawn.

The high percentage of unburned carbon in the ash and the large amount of ash and refuse rejected from the producer are a result of too frequent cleaning and poking of the fire and show inefficient firing. The behavior of the engine is accounted for by a poor quality of gas irregularly supplied. The amount of coal burned per B.H.P. hour, 1.62 lb., is much too high.

The load on the engine is less than half of normal rating thus decreasing to a great extent both the thermal and mechanical efficiency. During the brake test for the determination of mechanical efficiency of the engine the indicator on Cylinder No. 2 was out of commission and the total I.H.P. had to be estimated from the previous performance. The mechanical efficiency of the engine as obtained was 78.6%.

The pump was not worked to its full capacity due to the fact that the screen over the end of the intake pipe shut off one fourth of the opening; this also often became clogged; reducing still further the effective area. This condition impairs the efficiency to a very considerable extent and at normal load reduces the capacity of the pump. The velocity of water

in the pipe 7.85 feet per second was lower than normal capacity demands.

The column of normal results to be expected, shown under "Summary of Results" shows a wide variation from those actually obtained.

WILLIAM STREET
 DRIVEN 26" GENT
 DRAINAGE DIST
 IN ILLINOIS

NO	VEL IN FEET			
	12.5	25.0	37.5	50.0
1	64.1	1.13	1.00	1.065
2	67.4	1.13	.96	1.045
3	66.3	1.13	.93	1.03
4	65.5	.905	.96	.932
5	62.8	.905	.98	.942
6	62.5	.905		
7	55.0	1.13		
8	57.5	.905		
9	56.0			
10	62.0	1.13		
11	68.5		.71	
12	67.0		.85	
13	68.6			
14	68.0		.83	
15	65.0		.96	
16			.98	
17	61.4		.96	
18	59.5		1.00	
19	54.7		1.02	
20	41.4		.67	
21	55.6		.79	
22	51.7		.77	
23	48.4		.77	
24	44.1		.54	
25	60.0	1.13	.67	.90
26	60.1	1.13	.67	.90
27	60.3	1.35	1.04	1.195

5:46
7 hours, 24 min.
March 25, '08

11:10 P.M.

TEMP

Mechanical Efficiency
28.4
of Pump
Clear & windy.

17 Feet

P.M.	5:46	70.0	72	55	102	47	70	180	540	82.4	300	222	150	20.4	22.0	31.1	24.5	17.9	18.9	27.3	64.1	1.13	1.00	1.065	4.52	5.10	9.62	8.08	27.9	12,530	753,000	18,080,000	30.6	25.6	.84	.610
	5:55	69.5	72	55	101	46	68	207	540		300	222	150	23.2	19.6	34.0	25.6	20.4	17.2	29.8	67.4	1.13	.96	1.045	4.52	4.88	9.40	8.08	27.3	12,280	736,000	17,700,000	29.2	25.1	.86	.552
	6:00			55	101	46	68	222	540		300	222	150	22.7	19.0	33.9	25.2	20.0	16.6	29.7	66.3	1.13	.93	1.03	4.52	4.88	9.40	8.08	27.1	12,130	730,000	17,500,000	28.8	24.8	.86	.456
	10	70.0	72	55	104	49	66	198	540		292	216	146	23.6	19.4	33.7	25.6	20.2	16.5	28.8	65.5	.905	.96	.932	4.30	4.75	9.05	8.08	27.4	12,280	737,000	17,700,000	28.0	25.0	.894	.566
	20			50	101	51	70	190	540		288	213	144	23.6	20.6	30.6	24.9	20.0	17.2	25.6	62.8	.905	.98	942	3.96	4.75	8.71	8.08	28.8	12,920	776,000	18,600,000	28.5	26.4	.922	.584
	30	69.0	72	55	106	51	70	195	540		284	210	142	23.6	19.6	32.3	25.2	19.6	16.2	26.7	62.5	.905			3.96	4.75	8.71	8.08							.922	
	40			55	98	43	71	229	540	101.5	262	194	131	21.6	20.5	29.0	23.9	16.5	16.3	22.2	55.0	1.13			4.20	4.75	8.95	8.08							.903	
	50			55	97	42	71	222	540	86.	280	207	140	21.1	19.8	29.4	23.4	17.3	16.2	24.0	57.5	.905			3.96	4.75	8.71	8.08							.927	
	5:00	69.5	72.5	55	96	41	70	214	540		270	200	135	21.2	19.0	33.9	24.7	16.9	15.0	24.1	56.0				3.68	4.71	8.39	8.08							.965	
	10			54	99	45	71	201	540		292	216	146	23.2	19.0	30.5	24.2	19.8	16.2	26.0	62.0	1.13			3.96	4.65	8.61	8.08							.939	
	20			55	106	51	70	194	540		292	216	146	25.3	22.0	33.0	26.7	21.6	18.7	28.2	68.5		71		4.40	4.65	9.05	8.08	23.5	10,550	635,000	15,100,000	24.0	21.5	.899	.447
	30			54	109	55	70	194	540		295	218	147.5	25.6	19.7	32.4	25.9	22.1	16.9	28.0	67.0		85		4.40	4.65	9.05	8.08	25.8	11,550	694,000	16,600,000	26.4	23.6	.899	.576
	40			54	110	56	71	236	540		298	221	149	23.9	21.5	33.4	26.3	20.8	18.7	29.1	68.6				4.53	4.65	9.18	8.08							.88	
	50			54	111	57	70	250	53.5		300	222	150	26.0	19.8	31.8	25.9	22.8	17.3	27.9	68.0		83		4.53	4.65	9.18	8.08	25.5	11,450	688,000	16,500,000	26.6	23.4	.88	.502
	6:00	66.5	71	55	111	56	70	250	53.4		292	216	146	24.4	20.3	31.4	25.2	20.9	17.3	26.8	65.0		96		4.53	4.52	9.05	8.08	27.3	12,280	738,000	17,700,000	28.0	25.0	.894	.559
	10			54	107	53	70	270	53.0		290	215	145	24.4	20.1	31.4	25.3	20.7	17.0			.98			4.53	4.65	9.18	8.08	27.7	12,400	745,000	17,900,000	28.7	25.3	.88	
	20			54	112	58	70	280	53.0		286	212	143	22.7	20.4	30.4	24.5	19.0	17.0	25.4	61.4		.96		4.53	4.52	9.05	8.08	27.3	12,280	738,000	17,700,000	28.0	25.0	.894	.583
	30			54	105	51	71	284	53.0		284	210	142	22.0	19.6	30.2	23.9	18.3	16.2	26.0	59.5	1.00			4.30	4.58	8.88	8.08	27.9	12,530	753,000	18,080,000	28.2	25.6	.908	.605
	40				103	49	70	180	53.0		280	207	140	20.0	18.9			16.4	15.4	21.9	54.7	1.02			4.06	4.56	8.62	8.08	28.1	12,670	760,000	18,150,000	27.6	25.9	.938	.645
	50			99	45	70	160	53.0		260	193	130	19.6	17.0	28.0	21.5	14.9	12.9	13.6	41.4		.67		3.28	4.40	7.68	8.08	22.8	10,230	615,000	14,720,000	19.9	20.9	1.05	.605	
	7:00	66.0	70		96	42	70	168	52.9	85.5	270	200	135	19.6	19.3	31.5	23.5	15.5	15.2	24.9	55.6		.79		3.50	4.64	8.14	8.08	24.8	11,140	670,000	16,080,000	22.9	22.7	.994	.526
	10			54	95	41	70	172	52.9		268	199	134	19.4	17.3	29.7	22.1	15.2	13.5	23.0	51.7		.77		4.18	4.52	8.70	8.08	24.5	11,000	660,000	15,830,000	24.2	22.5	.93	.599
	20				98	44	70	168	52.9		260	193	130	16.0	18.8	29.0	21.3	12.2	14.2	22.0	48.4		.77		3.40	4.41	7.81	8.08	24.5	11,000	660,000	15,830,000	21.9	21.0	1.03	.579
	30				96	42	70	164	52.9		248	184	124	16.0	19.1	25.4	20.2	11.6	14.2	18.3	44.1		.54		3.28	4.41	7.69	8.08	20.6	9,230	555,000	13,300,000	17.9	18.8	1.05	.520
	8:30		68	54	82	28	70	180	53.0		292	216	146	20.7	20.3	29.2	23.4	17.7	17.3	26.0	60.0	1.13	.67	.90	4.06			8.08	22.8	10,230	615,000	14,750,000		20.9		
	40				84	30	68	198	53.0		284	210	142	20.0	23.8	28.8	24.2	16.7	19.6	23.8	60.1	1.13	.67	.90	4.06			8.08	22.8	10,230	615,000	14,750,000		20.9		
	50				86	32	68	195	52.9		280	207	140	22.0	20.9	30.7	24.5	18.1	17.1	25.1	60.3	1.35	1.04	1.195	4.06	5.75	9.81	8.08	27.3	12,280	736,000	17,700,000	30.4	25.0	.825	.695
	9:00	63.0	68		87	33	67	204	52.9	120.	284	210	142	17.9	23.3	31.5	24.2	14.9	19.3	26.0	60.2	1.33	1.03	1.180	4.18	5.36	9.54	8.08	28.3	12,750	766,000	18,380,000	30.7	26.0	.848	.652
	10				89	35	68	222	52.9		292	216	146	17.9	22.5	31.6	24.0	15.3	19.2	27.0	61.5	1.33	.96	1.145	4.30	5.10	9.40	8.08	27.3	12,250	736,000	17,700,000	29.1	25.0	.86	.605
	20				88	34	68	216	52.9		290	215	145	17.9	21.1	31.8	23.6	15.2	17.8	27.0	60.0	1.24	1.00	1.120	4.40	5.10	9.50	8.08	27.9	12,570	754,000	18,070,000	31.6	25.6	.85	.675
	30			53	88	35	68	210	52.6		288	213	144	22.0	21.1	32.0	25.0	18.5	17.7	26.9	63.1	1.18	1.04	1.110	4.45	5.20	9.65	8.08	28.5	12,800	768,000	18,450,000	31.4	26.1	1.21	.625
	40				88	35	66	219	52.3		284	210	142	22.0	23.8	27.1	24.3	18.3	19.7	22.4	60.4	1.13	1.04	1.085	4.52	5.30	9.82	8.08	28.5	12,800	768,000	18,450,000	31.7	26.1	.823	.672
	50				87	34	66	207	52.3		284	210	142	22.4	22.7	34.6	26.5	18.5	18.8	28.6	65.9	1.35	1.04	1.195	4.52	5.20	9.72	8.08	28.5	12,800	768,000	18,450,000	31.4	26.1	.831	.612
	10:00	60.5	68	53	89	36	66	214	52.3	154.	296	219	148	21.2	23.5	34.0	26.2	18.3	20.3	29.4	68.0	1.19	1.04	1.115	4.63	5.20	9.83	8.08	28.5	12,800	768,000	18,450,000	31.7	26.1	.822	.596
	10				89	36	67	202	52.2		290	215	145	21.2	22.5	32.1	25.2	17.9	19.0	27.2	64.1	1.30	1.04	1.170	4.63	5.25	9.88	8.08	28.5	12,800	768,000	18,450,000	31.8	26.1	.82	.637
	20				89	36	66	202	52.2		288	213	144	22.8	23.2	32.6	26.2	19.1	19.5	27.4	66.0	1.24	1.04	1.140	4.52	5.30	9.82	8.08	28.5	12,800	768,000	18,450,000	31.7	26.1	.823	.616
	30			53	88	35	67	208	52.2		284	210	142	22.8	24.1	34.6	27.1	18.9	19.9	28.6	67.4	1.24	1.08	1.160	4.52	5.20	9.72	8.08	29.1	13,052	784,000	18,800,000	32.3	26.6	.824	.615
	40				88	35	67	212	52.2	116.5	284	210	142	21.2	23.3	33.0	25.8	17.8	19.3	27.3	64.4	1.30	1.04	1.170	4.52	5.15	9.67	8.08	28.5	12,800	768,000	18,450,000	31.1	26.1	.838	.610
	50				89	36	67	210	52.2		284	210	142	20.7	24.3	30.7	25.2	17.2	20.0	25.4	62.6	1.35	1.02	1.185	4.52	5.15	9.67	8.08	28.2	12,680	760,000	18,250,000	32.0	26.8	.836	.634
	11:00	61.0	68	53	88	35	66	210	52.2	142.5	280	207	140	21.6	23.2	26.5	23.8	17.7	19.0	20.8	57.5	1.07	1.02	1.045	4.07	5.10	9.17	8.08	28.2	12,680	760,000	18,250,000	30.2	26.8	.881	.672
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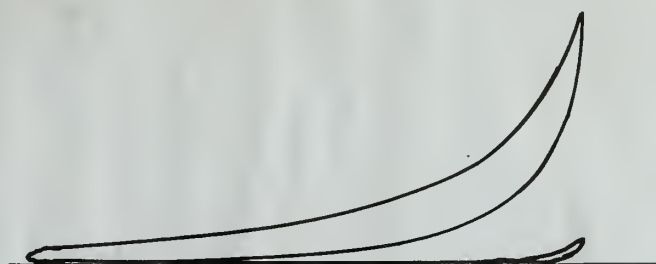
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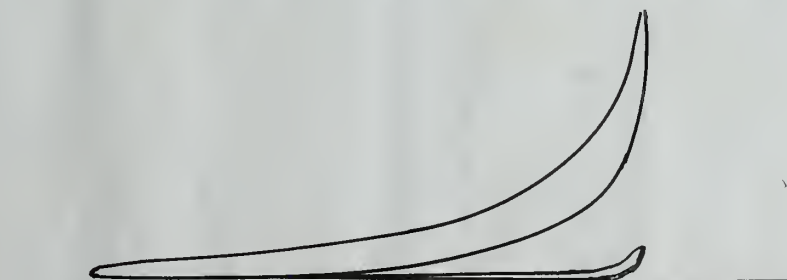
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PM	SEC	IN	OUT	DIFF	IN	OUT	IN	OUT	IN	OUT	IN	OUT	IN	OUT	IN	OUT
4:37		58	138	80	234		256	128	525	786	466	363	425	418	346	270
4:40		58	137	79	231		308	154	525	950	413	337	387	379	417	226
4:44		58	137	79	234		280	140	560	920	427	370	356	384	350	303
4:49		57	136	79	231		316	158	480	890	468	396	381	415	433	365
5:10		60	115	55			340	170	(75)	(15)						
5:20		60	120	59.5			316	158	205	380			257			242
5:24							310	155	235	426	368	323	299	330	333	292
5:28		60	110	50			316	158	225	418	356	410	186	317	328	378
5:30		60	110	50			256	128	425	640	400	347	335	361	297	258
5:33		59.5	110	50.5			290	145	430	730	417	299	400	372	344	253
5:37		60	122	620			288	144	440	742	418	290	411	373	344	243
5:40		59.5	144	84.5			292	146	555	950	493	373	474	446	419	317
							274	137	590	950	479	371	436	426	383	297
Total		650.5	1379	728.5	930		3842	1921	519.5	878.2	470.5	387.9	4097	422.1	3994	320.2
Average		59.1	125.3	66.2	232.5		296	148	432.9	732	428	352	372	38.4	36.3	29.1
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Cylinder No. 1



Cylinder No. 2



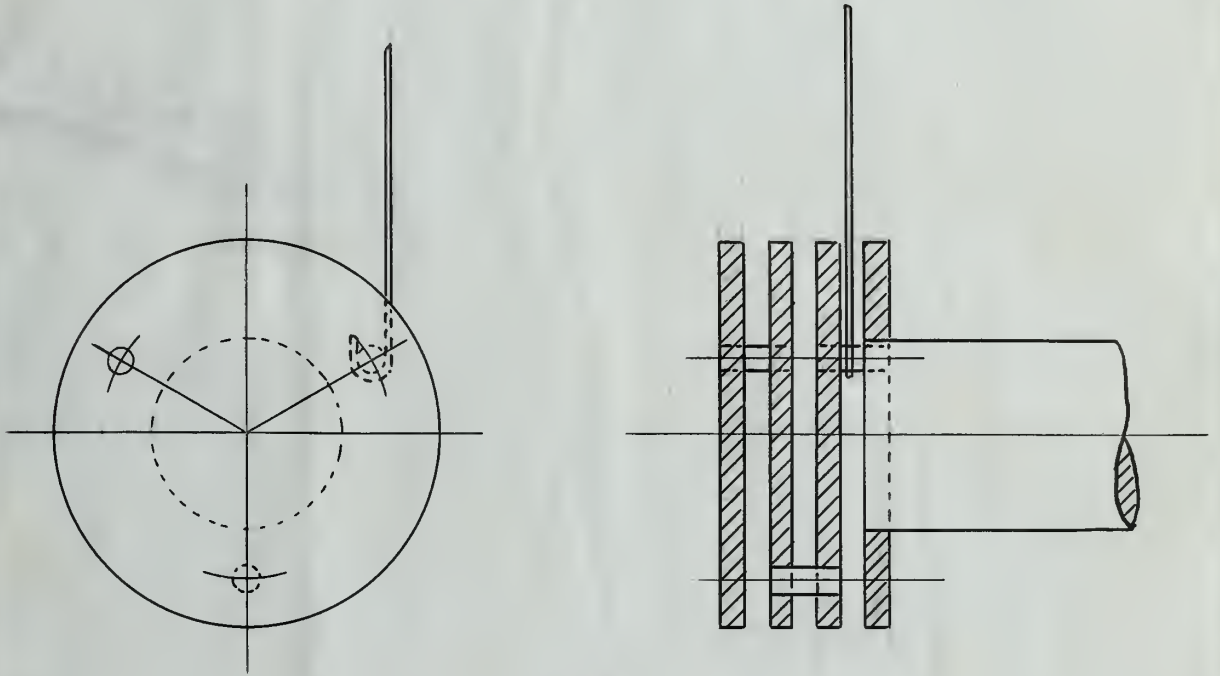
Cylinder No. 3

Indicator Diagrams No. 33

Test No. 1, Trial No. 2

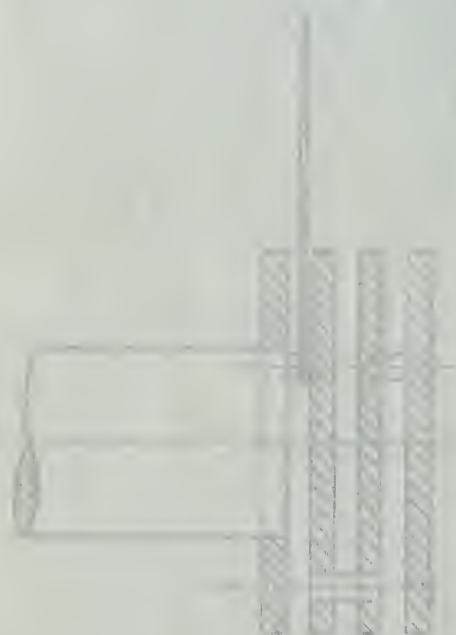
March 26, 1908

PeKin, Ill.

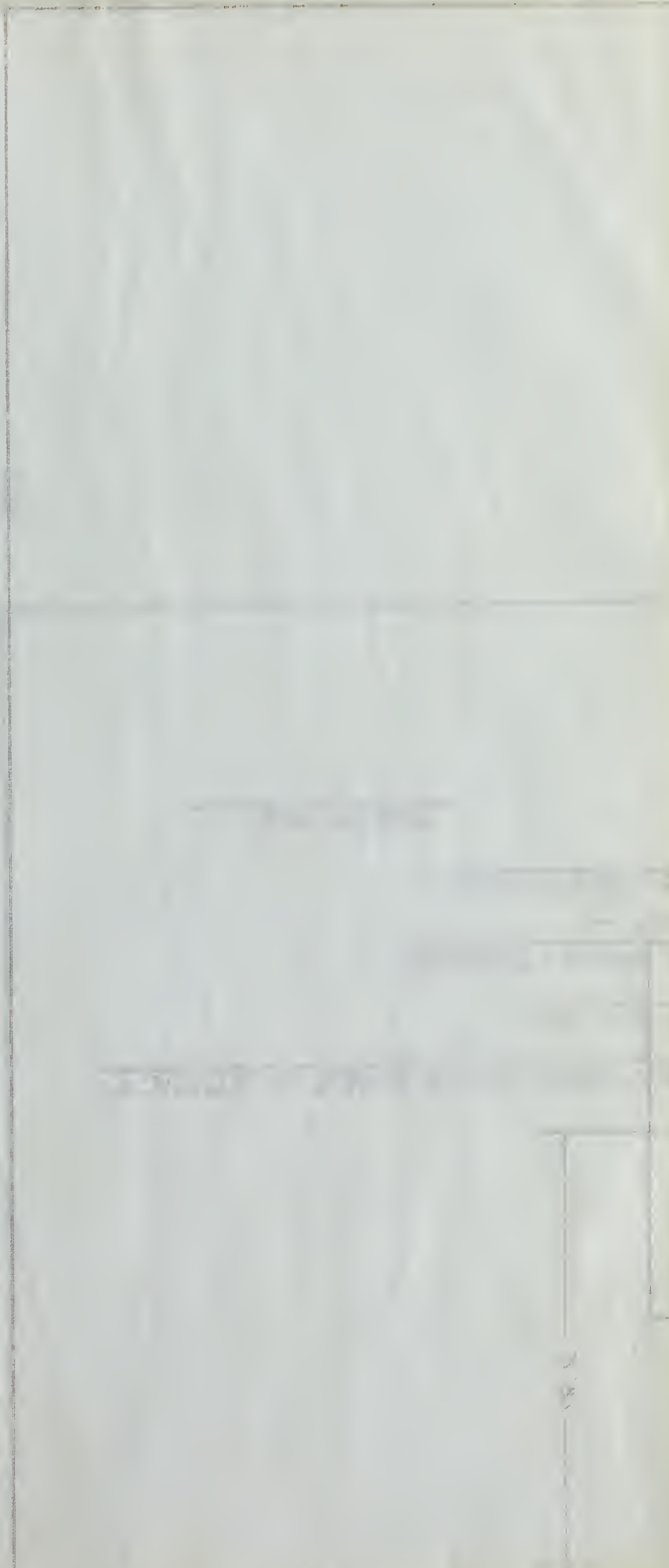
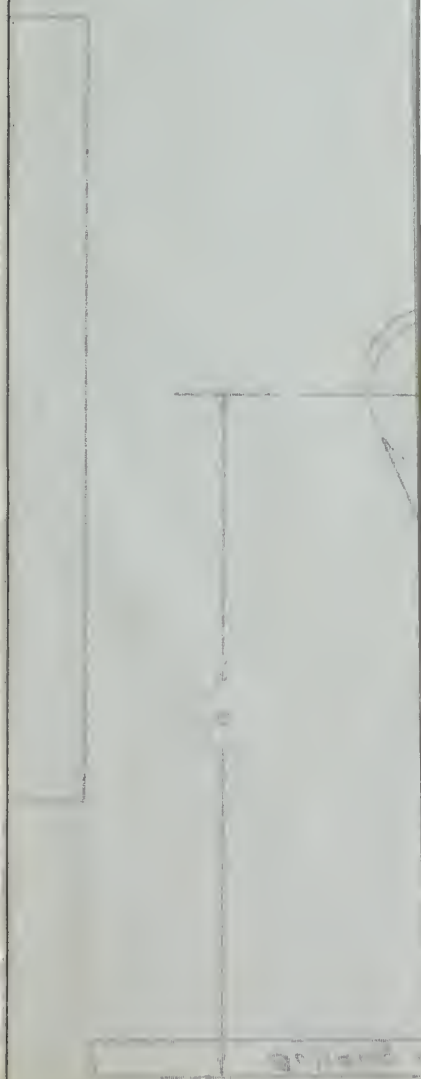
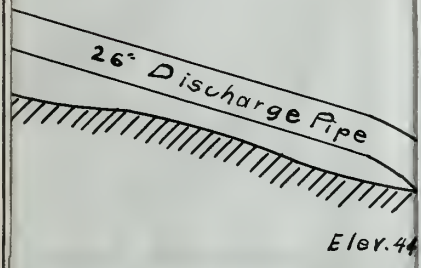


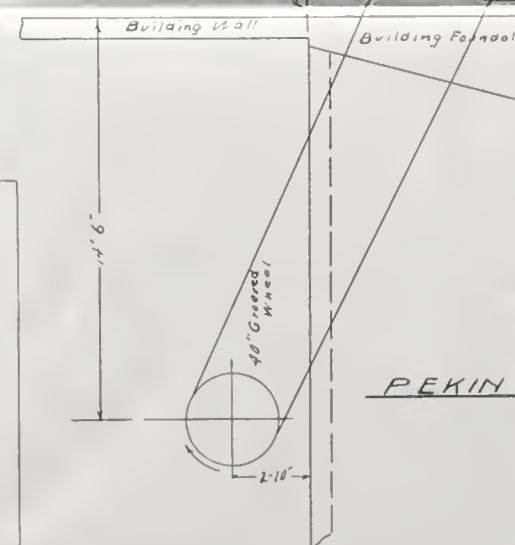
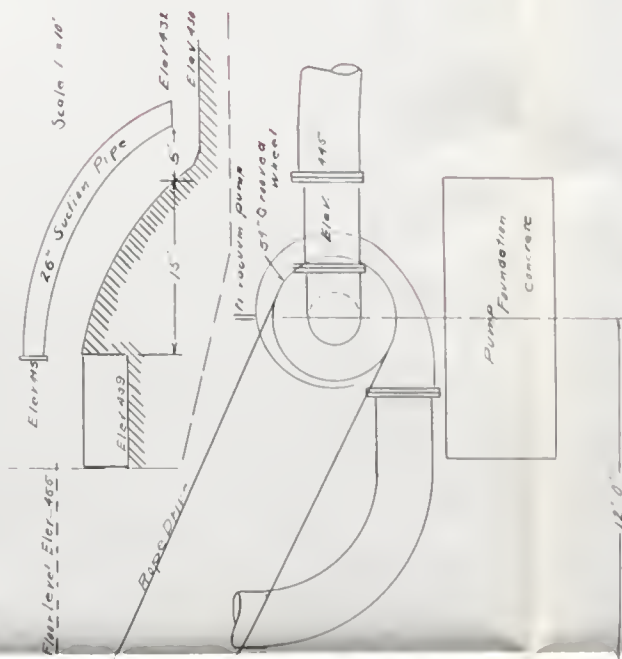
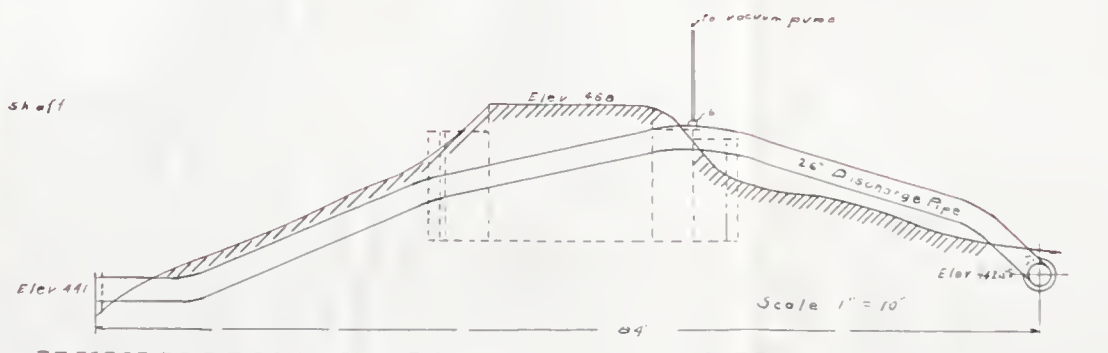
REDUCING MOTION

REDUCING MOTION



vum pump





May 21 1907.



UNIVERSITY OF ILLINOIS-URBANA



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